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- (72) Inventor; and
(71) Applicant : PIENAAR, Schalk Willem [ZA/ZA]; PO
Box 262, Wellington, 7654 (ZA).
- (74) Agent: Sibanda & Zantwijk; PO Box 1615, Houghton,
2041, Johannesburg Gauteng (ZA).
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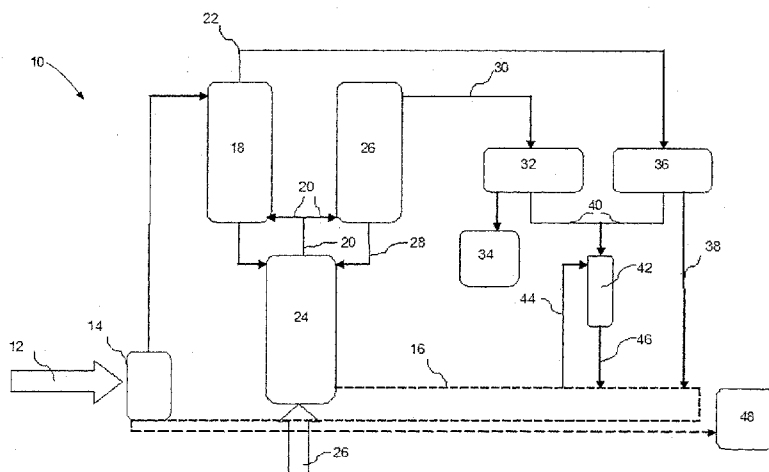
Declarations under Rule 4.17:

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- of inventorship (Rule 4.17(iv))

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(54) Title: PROCESS



(57) Abstract: The present invention refers to a process for reducing alcohol in a fermented beverage comprising (i) pre-heating a fermented beverage feedstock to a temperature between 40°C and 60°C, (ii) introducing said feedstock into the upper section of a distillation column operating at a pressure between 5kPa and 50kPa and a temperature between 40°C and 80°C, (iii) subjecting the feedstock, as it flows down the column, to alcohol vapour rising up the column, thereby stripping aromatics from the feedstock to yield an aromatic vapour. The aromatics are condensed. The fermented beverage is introduced into the upper section of a second distillation column operating at a pressure between 5kPa and 50 kPa and a temperature between 45 °C and 85°C and is subjected to steam/low-concentration alcohol vapour. The resulting alcohol vapour is transferred to a rectifier and is concentrated there. The fermented beverage is discharged from the second distillation column and mixed with the condensed aromatics.

WO 2013/177600 A1

PROCESS AND APPARATUS FOR THE REDUCTION OF ALCOHOL IN FERMENTED BEVERAGES

BACKGROUND

The present invention relates to a process and apparatus for the reduction of alcohol in fermented beverages. More particularly, the present invention relates to a process and apparatus for reducing the alcohol (i.e. ethanol) content of wine.

The challenge when reducing the alcohol content of wine is to:

1. not cause heat damage to the wine;
2. cause minimal water loss from the wine during the alcohol reduction process; and
3. retain in, or return to the wine as much aromatics and flavour components as possible.

In most wine producing countries, it is illegal to dilute wine with water. It is generally not illegal to adjust the taste of wine by removing constituents like acids. Except for a few countries, it is generally not illegal to remove alcohol from wine. It has become standard practice in hot climates, where grapes develop high sugar levels (and therefore, high alcohol content), to practise alcohol reduction techniques on the wine produced.

A variety of processes for removing select component parts from beverages are known. For example, evaporation technology is generally used to remove water from fruit juice and thereby concentrate the fruit juice. However, no feedback loop to re-introduce water evaporated from the feedstock fruit juice back into the evaporation chamber exists, causing the feedstock fruit juice to concentrate, and the operating temperature in the evaporation chamber consequently to rise. Drawbacks of evaporation chambers are that they result in significant water loss from the feedstock juice and their operating temperatures would cause heat damage to a wine feedstock.

Other technologies directed specifically at the removal of alcohol are also known. An example is the membrane processes, which extracts an alcohol-rich permeate stream from wine under pressure. Drawbacks of this process are that: the equipment is expensive; the membranes have a limited lifespan; and the high pressure required makes this process

energy intensive. A further example is the spinning cone column used by ConeTech, in which the wine is subjected to low-pressure heating in a column equipped with fast-rotating cones to drive off a portion of the alcohol. A drawback of this process is that, in addition to removing alcohol, many of the flavour components are also removed from the wine and need to be recovered and added back to the wine if the original flavour profile of the wine is to be retained. Another drawback is the inability of the ConeTech technology to concentrate the alcohol stream removed from the wine, resulting in undesirable loss of water from the de-alcoholised wine. A further drawback of the ConeTech technology is that its column includes many internal moving parts rotating at high speed, making the equipment expensive and energy and maintenance intensive.

The process and apparatus according to the present invention aims to address the above drawbacks and challenges.

SUMMARY OF THE INVENTION

According to a first aspect of the present invention there is provided a process for reducing alcohol in a fermented beverage that includes the steps of:

pre-heating a fermented beverage feedstock to a temperature between 40°C and 60°C;

introducing the pre-heated fermented beverage feedstock into the upper section of a first distillation column having an operating pressure between 5 kPa and 50 kPa and an operating temperature between 40°C and 80°C;

subjecting the fermented beverage feedstock, as it flows down the first distillation column, to alcohol vapour rising up the first distillation column, thereby stripping aromatics from the fermented beverage feedstock to yield an aromatic vapour;

passing the aromatic vapour through a first condenser to condense the aromatics from the aromatic vapour;

discharging the fermented beverage from the first distillation column;

introducing the fermented beverage discharged from the first distillation column into the upper section of a second distillation column having an operating pressure between 5 kPa and 50 kPa and an operating temperature between 45°C and 85°C;

subjecting the fermented beverage, as it flows down the second distillation column, to steam rising up the second distillation column, thereby stripping alcohol from the fermented beverage to yield an alcohol vapour;

splitting the alcohol vapour exiting the second distillation column into at least two streams, and feeding: (i) a first stream of alcohol vapour into the bottom section of the first distillation column; and (ii) a second stream of alcohol vapour into a rectifier;

refluxing the second stream of alcohol vapour in the rectifier to increase its alcohol concentration;

passing the refluxed alcohol vapour exiting the rectifier through a second condenser to condense the alcohol from the alcohol vapour;

returning at least a portion of the liquid condensed in the rectifier into the upper section of the second distillation column; and

discharging the fermented beverage from the second distillation column and returning at least a portion of the condensed aromatics thereto.

The process may include the step of subjecting at least a portion of the aromatics exiting the first condenser to a membrane separation process to remove a portion of the alcohol therefrom. And, at least a portion of the aromatics that has passed through the membrane separation process may be returned to the fermented beverage discharged from the second distillation column.

Typically, the steam rising up the second distillation column is a low concentration alcohol vapour between 1% and 50% ABV.

Preferably, the process includes the step of passing the vapours exiting the first and/or second condensers through a scrubber column. More preferably, at least a portion of the fermented beverage that has been discharged from the second distillation column is fed through the scrubber column to absorb aromatics from the vapours.

Typically, at least a portion of the fermented beverage with absorbed aromatics exiting the scrubber column is returned to the fermented beverage discharged from the second distillation column.

Generally, the fermented beverage is wine.

Preferably, the wine discharged from the second distillation column has an alcohol concentration greater than 1% alcohol-by-volume (ABV). More preferably, the wine discharged from the second distillation column has an alcohol concentration greater than 0.5% ABV.

Typically, the wine discharged from the second distillation column with aromatics re-introduced is mixed with fermented beverage feedstock and stored in a tank, packaged or bottled for human consumption.

According to a second aspect of the present invention there is provided apparatus for reducing alcohol in a fermented beverage using the process described above.

BRIEF DESCRIPTION OF THE DRAWINGS

A preferred embodiment of the invention will now be described in more detail, by way of example only, with reference to the accompanying drawing in which:

Figure 1 is a schematic diagram of a plant operating the process according to a preferred embodiment of the invention.

In this specification, "alcohol vapour" means vapour that includes both alcohol and water components. The term is not limited to pure alcohol vapour. Furthermore, all pressures mentioned in this specification are "absolute pressures".

DESCRIPTION OF THE INVENTION

With reference to the Figure 1, a process for reducing alcohol in a fermented beverage 10, such as wine, according to a preferred embodiment of the invention includes the steps of: (i)

removing aromatics from the wine; (ii) removing alcohol from the wine; (iii) refluxing a portion of the alcohol removed from the wine to increase the alcohol concentration of the alcohol vapour and return at least a portion of the condensed/recovered water to the wine; and (iv) condensing the aromatics removed from the wine and returning at least a portion thereof to the wine.

The process 10 starts by passing wine feedstock 12 through a pre-heater 14 to pre-heat the wine feedstock 12 to a temperature between 40°C and 60°C. The pre-heater 14 transfers heat from de-alcoholised wine 16 that has previously passed through the process 10.

The pre-heated wine feedstock 12 is then introduced into a first distillation column 18 through an inlet at or near the top of the column and permitted to flow under gravity to the bottom of the column 18. At or near the bottom of the first distillation column 18 is an inlet for alcohol vapour 20 to enter and rise up the column 18 to a vapour outlet near the top of the column 18. The counter-flow of the wine feedstock 12 travelling down the column 18 and the alcohol vapour 20 rising up the column 18 causes aromatics (together with a small amount of alcohol and water) to be stripped from the wine feedstock 12 to yield an aromatic vapour 22. The degree of stripping of aromatics from the wine feedstock 12 is determined by the rate of flow of alcohol vapour 20 through the first distillation column 18, as controlled by a valve (not shown) in either the alcohol vapour inlet or the vapour outlet. The interior of the first distillation column 18 typically includes random or structured packing or trays (not shown) to encourage aromatic stripping of the wine feedstock 12 by the alcohol vapour 20.

To prevent heat damage to the wine 12, the first distillation column 18 operates at a pressure between 5 kPa and 50 kPa and a temperature between 40°C and 80°C – the temperature being dependent on the pressure in the first distillation column.

The de-aromatized wine collected at the bottom of the first distillation column 18 is discharged from the column 18 and introduced into a second distillation column 24 through an inlet at or near the top of the second distillation column 24 and permitted to flow under gravity to the bottom of the column 24. At or near the bottom of the second distillation column 24 is an inlet for low pressure steam or low concentration alcohol vapour (i.e. between 1% and 50% alcohol-by-volume (ABV)) 26 to enter and rise up the column 24 to a vapour outlet near the top of the column 24. The counter-flow of the de-aromatized wine 12 travelling down the column 24 and the steam / low-concentration alcohol vapour 26 rising up the column 24 causes alcohol (together with some water and residual aromatics) to be

stripped from the de-aromatized wine 12 to yield an alcohol vapour stream 20 having an alcohol concentration typically between 40% to 70% ABV (dependent on the alcohol concentration of the wine feedstock 12). The degree of stripping of alcohol from the de-aromatized wine 12 is determined by the rate of flow of steam / low-concentration alcohol vapour 26 through the second distillation column 24. The steam / low-concentration alcohol vapour 26 is generated by partial vaporisation of a portion of the de-alcoholised wine 16 in the base of the second distillation column 24. This enables the production of wine with a varying degree of alcohol depletion exiting the bottom of the second distillation column 24. The interior of the second distillation column 24 typically includes random or structured packing or trays (not shown) to encourage alcohol stripping of the de-aromatized wine 12 by the steam / low concentration alcohol vapour 26.

To prevent heat damage to the wine 12, the second distillation column 24 operates at a pressure between 5 kPa and 50 kPa and a temperature between 45°C and 85°C

The alcohol vapour 20 exiting the second distillation column 24 is split into two streams. A first stream 20 is fed into the first distillation column 18 via the alcohol vapour inlet and a second stream 20 is fed into a rectifier 26. While in the rectifier 26, the second stream of alcohol vapour 20 encounters refluxed alcohol liquid, continually condensing and evaporating until the alcohol concentration of the alcohol vapour 20 within the rectifier 26 reaches typically 80% to 95% ABV. The reflux process increases the alcohol content of the alcohol vapour 20 by condensing water therefrom. This water 28 (with an alcohol component) is collected at the bottom of the rectifier 26 and returned to the top of the second distillation column 24. In so doing, the water 28 condensed from the alcohol vapour 20 in the rectifier 26 is returned to the de-aromatized wine 12 in the second distillation column 24.

The alcohol vapour 30 exiting the rectifier 26 is passed through a second condenser 32 that uses a cold utility, cooling water, chilled water, or glycol to condense the alcohol therefrom, which is stored in a tank 34.

De-alcoholised wine 16 discharged from the second distillation column 24 has an alcohol concentration greater than 1% ABV or, in some instances, 0.5% ABV. This de-alcoholised wine 16 is returned to the pre-heater 14 to transfer heat to wine feedstock 12 and thereby reduce the temperature of the de-alcoholised wine 16 to between 20°C and 40°C, depending on the temperature of the wine feedstock 12.

The aromatic vapour 22 exiting the first distillation chamber 18 is passed through a first condenser 36 (which typically operates at a temperature 1 to 5°C higher than that of the second condenser 32) to condense the aromatics from the aromatic vapour 22, which condensed aromatics 38 (or a portion thereof) are then returned to the de-alcoholised wine 16.

The vapour 40 exiting the first and second condensers 32 and 36 is then passed through a scrubber column 42 that is fed 44 by at least a portion of the de-alcoholised wine 16 to absorb residual aromatics from the vapour 40.

At least a portion of the wine (with absorbed aromatics) 46 exiting the scrubber column 42 is then returned to the de-alcoholised wine 16.

Optionally, at least a portion of the condensed aromatics 38 exiting the first condenser 36 may be subjected to a membrane separation process to remove a portion of the alcohol therefrom. And, at least a portion of the condensed aromatics 38 that has passed through the membrane separation process may be returned to the fermented beverage discharged from the second distillation column 24.

By returning water 28 to the de-aromatized wine in the second distillation column 24 and aromatics 38 and 46 to the de-alcoholised wine 16, the de-alcoholised wine 16 retains many of its flavour components despite having its alcohol content reduced.

The de-alcoholised wine 16 with aromatics 38 and 46 re-introduced is then mixed with wine feedstock 12 (that has not been pre-heated) and stored in a tank 48, packaged or bottled for ultimate human consumption. For example, mixing 25% de-alcoholised wine 16 having an alcohol concentration of 1% ABV with 75% wine feedstock 12 having an alcohol concentration of 16% ABV yields a wine with an alcohol concentration of 14.5% ABV.

The process 10 is a single, continuous process using distillation columns 18 and 24 having no internal moving parts.

A second aspect of the invention relates to apparatus used in the process 10 described above.

It will be appreciated that, although the process 10 has been described using wine as a feedstock 12, any other fermented beverage can be used as a feedstock.

It will also be appreciated that the flow of wine 12 and 16 during the process 10 can be caused by pumps or gravity employing a double-lock (air-lock type) arrangement to enable draining against the force of the operating vacuum in the distillation columns 18 and 24 and rectifier 26.

CLAIMS

1. A process for reducing alcohol in a fermented beverage including the steps of:

pre-heating a fermented beverage feedstock to a temperature between 40°C and 60°C;

introducing the pre-heated fermented beverage feedstock into the upper section of a first distillation column having an operating pressure between 5 kPa and 50 kPa and an operating temperature between 40°C and 80°C;

subjecting the fermented beverage feedstock, as it flows down the first distillation column, to alcohol vapour rising up the first distillation column, thereby stripping aromatics from the fermented beverage feedstock to yield an aromatic vapour;

passing the aromatic vapour through a first condenser to condense the aromatics from the aromatic vapour;

discharging the fermented beverage from the first distillation column;

introducing the fermented beverage discharged from the first distillation column into the upper section of a second distillation column having an operating pressure between 5 kPa and 50 kPa and an operating temperature between 45°C and 85°C;

subjecting the fermented beverage, as it flows down the second distillation column, to steam rising up the second distillation column, thereby stripping alcohol from the fermented beverage to yield an alcohol vapour;

splitting the alcohol vapour exiting the second distillation column into at least two streams, and feeding: (i) a first stream of alcohol vapour into the bottom section of the first distillation column; and (ii) a second stream of alcohol vapour into a rectifier;

refluxing the second stream of alcohol vapour in the rectifier to increase its alcohol concentration;

passing the refluxed alcohol vapour exiting the rectifier through a second condenser to condense the alcohol from the alcohol vapour;

returning at least a portion of the liquid condensed in the rectifier into the upper section of the second distillation column; and

discharging the fermented beverage from the second distillation column and returning at least a portion of the condensed aromatics thereto.

2. A process for reducing alcohol in a fermented beverage according to claim 1, further including the step of subjecting at least a portion of the aromatics exiting the first condenser to a membrane separation process to remove a portion of the alcohol therefrom.
3. A process for reducing alcohol in a fermented beverage according to claim 2 further including the step of returning at least a portion of the aromatics that has passed through the membrane separation process to the fermented beverage discharged from the second distillation column.
4. A process for reducing alcohol in a fermented beverage according to either claim 1 or claim 3, wherein the steam rising up the second distillation column is a low concentration alcohol vapour.
5. A process for reducing alcohol in a fermented beverage according to claim 4, wherein the low concentration alcohol vapour is between 1% and 50% ABV.
6. A process for reducing alcohol in a fermented beverage according to claim 5 further including the step of passing the vapours exiting the first and/or second condensers through a scrubber column.
7. A process for reducing alcohol in a fermented beverage according to claim 6 further including the step of feeding at least a portion of the fermented beverage that has been discharged from the second distillation column through the scrubber column to absorb aromatics from the vapours.
8. A process for reducing alcohol in a fermented beverage according to claim 7 further including the step of returning at least a portion of the fermented beverage with

absorbed aromatics exiting the scrubber column to the fermented beverage discharged from the second distillation column.

9. A process for reducing alcohol in a fermented beverage according to any one of the preceding claims, wherein the fermented beverage is wine.
10. A process for reducing alcohol in a fermented beverage according to claim 9, wherein the alcohol concentration in the wine discharged from the second distillation column is greater than 1% alcohol-by-volume.
11. A process for reducing alcohol in a fermented beverage according to claim 10, wherein the alcohol concentration in the wine discharged from the second distillation column is greater than 0.5% alcohol-by-volume.
12. A process for reducing alcohol in a fermented beverage according to any one of claims 9 to 11, wherein the process includes the further step of mixing wine discharged from the second distillation column with aromatics re-introduced with fermented beverage feedstock.
13. A process for reducing alcohol in a fermented beverage according to any one of claims 9 to 12, further including the step of storing, packaging or bottling the mixed wine.
14. Apparatus for reducing alcohol in a fermented beverage using the process described in any one of claims 1 to 13.

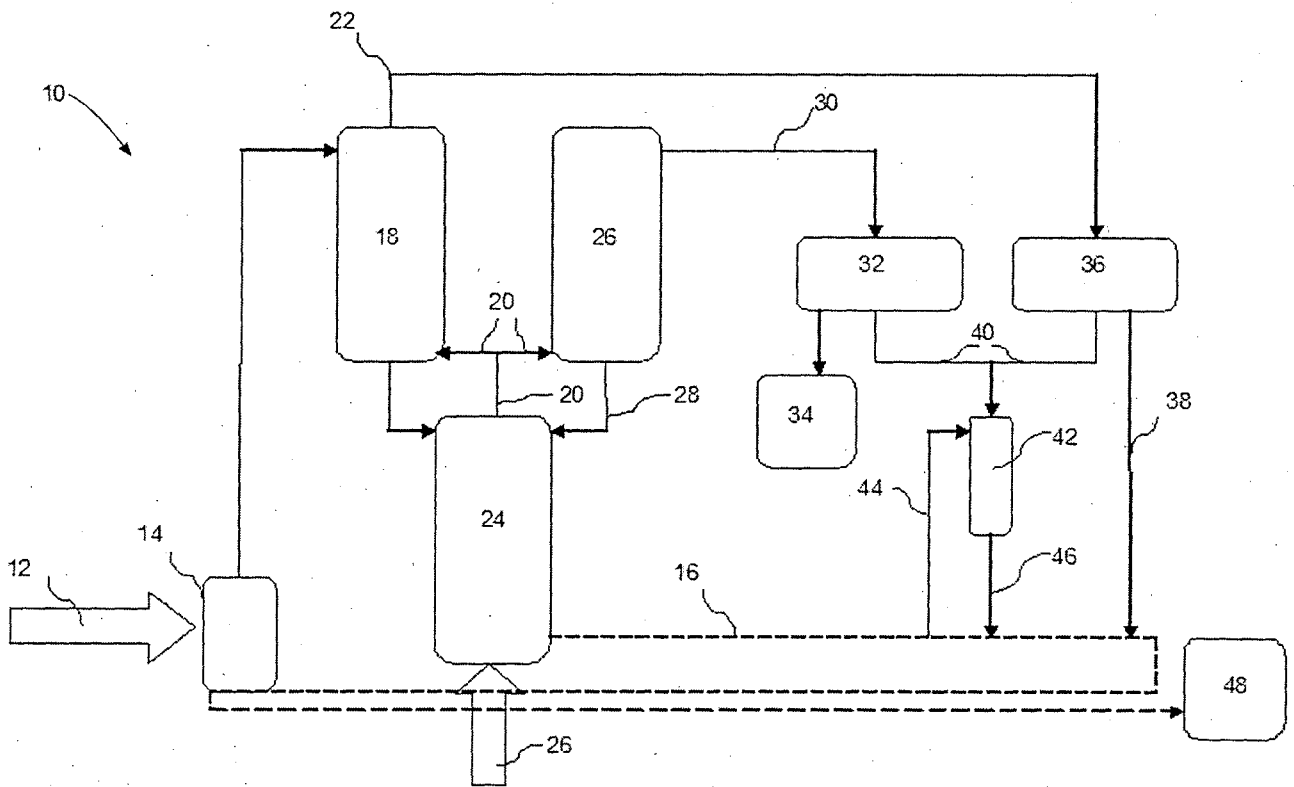


Figure 1

INTERNATIONAL SEARCH REPORT

International application No.

PCT / ZA 2013/000022

<p>A. CLASSIFICATION OF SUBJECT MATTER IPC: C12G 3/08 (2006.01) According to International Patent Classification (IPC) or to both national classification and IPC</p>		
<p>B. FIELDS SEARCHED Minimum documentation searched (classification system followed by classification symbols) C12G Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched</p>		
<p>Electronic data base consulted during the international search (name of data base and, where practicable, search terms used) WPI, EPODOC</p>		
<p>C. DOCUMENTS CONSIDERED TO BE RELEVANT</p>		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0768373 A2 (NEWHAVEN PROPERTIES LIMITED) 16 April 1997 (16.04.1997) whole document	1-12
A	GB 2084607 A (AG PATENTS LTD) 15 April 1982 (15.04.1982) whole document	1-12
A	DE 3819527 A1 (GEA WIEGAND GMBH & CO, 7505 ETTLINGEN, DE) 21 December 1989 (21.12.1989) whole document	1-12
A	EP 0058634 A1 (SCHWEIZERISCHE EIDGENOSSENSCHAFT HANDELND DURCH DIE EIDG.FORSCHUNGSANSTALT FUER OBST-, WEIN- UND GAR) 25 August 1982 (25.08.1982) whole document	1-12
<p><input type="checkbox"/> Further documents are listed in the continuation of Box C. <input checked="" type="checkbox"/> See patent family annex.</p>		
<p>* Special categories of cited documents:</p> <p>“A” document defining the general state of the art which is not considered to be of particular relevance</p> <p>“E” earlier application or patent but published on or after the international filing date</p> <p>“L” document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>“O” document referring to an oral disclosure, use, exhibition or other means</p> <p>“P” document published prior to the international filing date but later than the priority date claimed</p> <p>“T” later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>“X” document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone</p> <p>“Y” document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art</p> <p>“&” document member of the same patent family</p>		
<p>Date of the actual completion of the international search 21 June 2013 (21.06.2013)</p>		<p>Date of mailing of the international search report 01 July 2013 (01.07.2013)</p>
<p>Name and mailing address of the ISA/AT Austrian Patent Office Dresdner Straße 87, A-1200 Vienna Facsimile No. +43 / 1 / 534 24-535</p>		<p>Authorized officer KRENN M. Telephone No. +43 / 1 / 534 24-435</p>

Box No. II Observations where certain claims were found unsearchable (Continuation of item 2 of first sheet)

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. Claims Nos.:

because they relate to subject matter not required to be searched by this Authority, namely:

2. Claims Nos.: 13, 14

because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:

Storing, packaging or bottling wine are not steps belonging to a process for reducing alcohol in a fermented beverage; thus said features are not suitable for characterizing the presently claimed process (claim 13).

Claim 14 lacks disclosure of structural features of the claimed apparatus. An apparatus can however only sufficiently described by its components.

3. Claims Nos.:

because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box No. III Observations where unity of invention is lacking (Continuation of item 3 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1. As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.

2. As all searchable claims could be searched without effort justifying additional fees, this Authority did not invite payment of additional fees.

3. As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:

4. No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

The additional search fees were accompanied by the applicant's protest and, where applicable, the payment of a protest fee.

The additional search fees were accompanied by the applicant's protest but the applicable protest fee was not paid within the time limit specified in the invitation.

No protest accompanied the payment of additional search fees.

INTERNATIONAL SEARCH REPORT
Information on patent family members

International application No.

PCT / ZA 2013/000022

Patent document cited in search report			Patent family member(s)			Publication date
EP	A2	0768373	ES	T3	2133901	1999-09-16
			DE	T2	69602155	1999-11-25
			EP	A2	0768373	1997-04-16
			GR	T3	3030812	1999-11-30
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DE	A1	3819527	DE	A1	3819527	1989-12-21
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			CH	A5	654023	1986-01-31
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			WO	A1	8202723	1982-08-19
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			HU	B	185461	1985-02-28
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			US	A	4626437	1986-12-02